

1	CUSTOMER	SAMSUNG HEAVY INDUSTRIES			REFERENCE NO.	Golar						
2	ADDRESS				CPP FILE NO.	CPP-11-104 (CH11-1234)						
3	PLANT LOCATION				DATE	January 31, 2012						
4	SERVICE OF UNIT	Single Stage H.P. LNG Vaporizer (SI Units)			ITEM NO.	HA 1100/2100/3100/ A/B						
5	SIZE	52648-1	TYPE	Special NJN	HORIZONTAL inclined 3 degrees							
6	SURFACE (m ²)	(GROSS) 789.8	SHELLS/UNIT	One	SURF/SHELL (m ²)	(NET)	770.3					
7	PERFORMANCE OF ONE UNIT											
8				SHELL SIDE		TUBE SIDE						
9	FLUID CIRCULATED				Sea Water		LNG / Natural Gas					
10	TOTAL FLUID ENTERING				2632 m ³ /hr (Note 1)		104,276.10 kg/hr					
11			INLET	OUTLET	INLET	OUTLET						
12	VAPOR	kg/hr	---	---	---	104,276.10						
13	LIQUID	kg/hr	2,697,610	2,697,610	104,276.10	---						
14	NON-CONDENSABLES	kg/hr	---	---	---	---						
15	DENSITY	kg/m ³	1026.51	1028.66	433.56	101.26						
16	VISCOSITY	cP	1.013	1.418	0.1186	0.0149						
17	SPECIFIC HEAT	kJ/kg-°C	3.9289	3.9333	3.6001	3.5279						
18	THERMAL CONDUCTIVITY	W/m-°C	0.6127	0.6023	0.1997	0.0518						
19	LATENT HEAT	kcal/kg										
20	MOLECULAR WEIGHT					16.72 (Note 4)						
21	TEMPERATURE IN	°C	14.0		-152.9							
22	TEMPERATURE OUT	°C	7.22 (Note 2)		8.0							
23	OPERATING PRESSURE	BarG	ONE		ONE							
24	NO. PASSES PER SHELL		ONE		ONE							
25	VELOCITY											
26	PRESSURE DROP	Bar	1.74 (Note 3)		0.43							
27	FOULING RESISTANCE	m ² -C/W	Note 5		Note 5							
28	HEAT EXCHANGED	19,934.99	kW		MTD CORRECTED	44.8 °C						
29	TRANSFER RATE - SERVICE	664.4 / 577.7	W/ m ² C		(Clean / Design)							
30	CONSTRUCTION											
31	DESIGN PRESSURE	BarG	7.0		125							
32	TEST PRESSURE	BarG	Per Code		Per Code							
33	DESIGN TEMPERATURE (Max/Min)	°C	65 / -170		65 / -195.5							
34	TUBES	254 SMO (Note 6)	NO	802	OD	0.75	BWG	16	LENGTH	16.46 m	PITCH	33.3375 mm
35	SHELL	AL6XN	ID		OD	132.1 cm						
36	EXPANSION JOINT (BELLOWS)	AL-6XN										
37	BONNET	316L SS		CHANNEL COVER		N/A						
38	TUBESHEET-STATIONARY	AL-6XN		TUBESHEET-FLOATING		N/A						
39	BAFFLES - CROSS	AL-6XN		TYPE	Seg.	FLOATING HEAD COVER		N/A				
40	TUBE SUPPORTS	AL-6XN		IMPINGEMENT PROTECTION		Yes						
41	GASKETS	N/A		PACKING		N/A						
42	TUBE TO TUBESHEET JOINT	Seal Welded & Rolled into Double Grooved Holes										
43	CONNECTIONS-SHELL SIDE	IN	QTY (2) 20" on 26" reducer	OUT	30"	RATING	16K JIS					
44	CONNECTIONS-TUBE SIDE	IN	8"	OUT	12"	RATING	900# RFWN					
45	CORROSION ALLOWANCE - SHELL SIDE	---		TUBE SIDE	---							
46	CODE REQUIREMENTS	ASME Sec. VIII, Div. 1			TEMA CLASS			"R"				
47	OTHER	DNV										
48	NOTES	(1) 1316 m ³ /hr in "Cold" LNG section & 1316 m ³ /hr in "Warm" NG section at full load										
49		(2) SW bulk outlet temperature. SW flow of 1303 m ³ /hr in the "Cold" LNG section should be maintained at all times to guard against potential freeze problems.										
50		(3) SW pressure drop when operating at full load.										
51		(4) Standard LNG: 98.01% C1, 3.2% C2, 0.6% C3, 0.05% iC4, 0.05% nC4, 0.01% iC5, 0.08% N2 (mole %)										
52		(5) 15% excess surface area with no additional fouling applied										
53		(6) Helium leak tested tube to tubesheet joints										
54		(7) The hot circuit must be started first and shut down last.										
55		(8) Proprietary design features for tube side LNG distribution, performance, and venting.										

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