



Procedure di Gestione Ambientale

Cod. PO CO₂

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UB - PC

Procedure Operative

Nome File
Allegato 9

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INTERNATIONAL STANDARD ISO 5167

PROGRAM: PIT-CAEF- 10

CALCOLO PER DISCHI TARATI A SPIGOLO VIVO
CALCULATION FOR SQUARE EDGE ORIFICES

FOGL./SHT.: J-3888/1

COMMESSA/JOB No	: J-3888	DATA/DATE	: 10.12.02
CLIENTE/CUSTOMER	: ENELPOWER SPA	ORDINE/ORDER	: I.AA.2.2.167.1
FLUIDO/STREAM	: METANO	SIGLA/TAG	: E-G-44B NQ399X
MODEL	: METER RUN	MATERIAL	: SS316+A106/B
SIZE	: 10"300RF	TYPE	: FLANGE TAPS-PRESE SULLE FLANGE

W = PORTATA M/FUL.SC.FLOW	: 65415.1	Kg/hr	84000	Nm ² /h	T1=TEMP.MONTE/UPST.TEMP.	: 35	°C	35	°C
Wh=PORT.NORM/NORMAL FLOW	: 52176.33	Kg/hr	67000	Nm ³ /h	Di=DI.INT.TUB/IN.PIPE DI.	: 253.5	mm	253.5	mm
P1=PRS.MONTE/UPSTR.PRES.	: 31.624	Kp/cm ² A	3000	KPa R	Zf=FAT.COMP/COMPRES.FACT.	: 1		1	
dP=PRES.DIFF./DIFF.PRESS.	: .25	Kp/cm ²	2500	mm H2O	Yb=PESO SP.RIF/REF.SPC.WT	: .7788	Kg/m ³	0	Kg/m ³
Pn=PRS=VALLE/DWNST.PRES.	: 31.374	Kp/cm ² A	0	KPa R	Yf=PESO SP.ES./FL.SPEC.WT	: 21.133	Kg/m ³	0	Kg/m ³
u = VISCOS.CIN/KIN.VISCOS.	: .473	cStk.	.01	cp	e = FAT.ESPANSIONE/EXPANS. FACTOR		.9982		
I = ENTALPIA/ENTHALPY	: 0	Kcal/Kg			k = ESPON.ADIAB/ADIAB.EXP.	: 1.4	cp/cv		
Fa=COEF.DIL/DIL.FACT.	: 1.0007				Mw=PESO MOLECOL./MOLECULAR WEIGHT		: 17.46		

$$\alpha B^2 = \frac{W}{1.251 \cdot Fa \cdot Di^2 \cdot \sqrt{dP} \cdot \sqrt{Yf} \cdot e} = \frac{65415.1}{1.251 \times 1.0007 \times 64262.25 \times .5 \times 4.5971 \times .9982} = .3544081$$

d	: 180.65	mm	DIAMETRO ORIFIZIO / ORIFICE DIAMETER
B = do/Di	: .712637		RAPPORTO DI STROZZAMEN. / ORIFICE TO PIPE RATIO
α = C.E	: .697863		COEFFICIENTE DI PORTATA / FLOW COEFFICIENT
C	: .6011704		COEFFICIENTI DI EFFLUSSO / COEFFICIENT OF DISCHARGE
E = f(1/(1-B ⁴))	: 1.160841		COEF.VELOC.DI APPROCCIO / VELOC.OF APPROACH FACT.
RD=10 ³ .Vp.Di/u	: 7282557 --		NUMERO DI REYNOLDS NORM./ NORMAL PIPE REYNOLDS No
V0	: 26.76	m/sec	VELOC.NORM.EFFLUSSO ORIF/ NORM.ORIF.OUTLET VELOC.
Vp	: 13.59	m/sec	VELOCITA'NORM. CONDOTTA / PIPE NORMAL VELOCITY
βP= 47.7 % dP	: .119		Kp/cm ² PERDITA DI CARICO PERMAN/ PERMANENT PRESS.LOSS

0 TRATTO MIN.TUBAZ.DIRITTA MONTE/VALLE	MIN.UPSTREAM/DOWNSTREAM STRAIGHT PIPE REQUIREMENT		
RACCORDI A MONTE	UPSTREAM FITTINGS	B=	{ 0.45 .45 -.55 .55 -.65 .65 -.73 } 0.73
RIDUZIONE < 0.5 Diam.	REDUCER < 0.5 Dia.	A= 6 B=5	A= 8 B=6 A=11 B=7 A=20 B=8 A=30 B=8
VALVOLA TUTTA APERTA	FULLY OPEN VALVE	A=20 B=6	A=23 B=6 A=27 B=7 A=34 B=7 A=40 B=8
1 GOMITO O CURVA	1 ELBOW OR BEND	A=12 B=6	A=16 B=6 A=21 B=7 A=34 B=7 A=42 B=8
2 CURVE STESSO PIANO	2 BENDS SAME PLANE	A=18 B=6	A=21 B=6 A=30 B=7 A=38 B=7 A=45 B=8
L1=A.Di=mm=TRATTO A MONTE/UPSTREAM RUN	L2=B.Di=mm=TRATTO A VALLE/DOWNSTREAM RUN		

CALCOLO DELL'ERRORE PROBABILE EXPECTED ERROR EVALUATION
 SCOSTAM. TIPO : a= σα = ± .71 % b= σDi = ± .5 % c= σd = ± .02 % d= σdP = ± 1.00 %
 STD.DEVIATION : e= σYf = ± 1 % f= σFa = ± .3 % g= β⁴/α = .37 % h= σe = ± .02 %
 PER CONDIZIONI ESERCIZIO ENTRO LE TOLLERANZE INDICATE FOR OPERATING CONDITIONS WITHIN INDICATED TOLERANCES

$$\sigma W = \sqrt{a^2 + (4 \cdot g^2 \cdot b^2) + \alpha^4 (1+g)^2 \cdot c^2 + 0.25(d^2 + e^2) + f^2 + h^2 \cdot e^{1/2}} = \pm 1.11 \%$$

Err.% = 2.σW = ± 2.22 % ERRORE PROBABILE / EXPECTED ERROR
 Add.Error = ± 0.5 % PER TRATTO DIR. (L1+L2) MA ≥ 0.5(L1+L2) / FOR STRAIGHT RUN (L1+L2) BUT ≥ .5(L1+L2)

** REYNOLDS No MIN. = 162212.7 ** REYNOLDS No MAX. = 10⁸